OPTIMIZATION OF ENZYME CATALYZED PEPTIDE SYNTHESIS IN A "WATER - WATER-IMMISCIBLE ORGANIC SOLVENT" BIPHASIC SYSTEM

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(Received in UK 6 April 1984)

Abstract - Optimal conditions were found for enzymatic synthe-ADMIT CONTRACT CONTRACT ON THE STATE OF STATES of the dipeptide, N-acetyl-L-tryptophanyl-L-leucine anide
in the biphasic system water - ethyl acetate. The synthesis
was carried out using both free and immobilized α -chym phase, which conditions the dipeptide was synthesized on the preparative scale in ca. 100% yield. As a result of immobili-
zation (adsorption on the Sorsilen terephtalate support) the enzyme practically did not inactivate and may be used repeatedly.

INTRODUCTION

Application of enzymes in fine organic synthesis appears very promising and in some instances is highly advantageous compared to conventional methods of chemical synthesis.¹⁻⁶ In particular, certain progress has been achieved in applying enzymes for the synthesis of peptides, see reviews.^{3,7-14}

Unfortunately, a broader application of enzymes in preparative organic synthesis is somewhat limited because of the fact that enzymes retain their catalytic properties only in a rather narrow range of conditions, viz. in aqueous solutions at pH close to neutral and at moderate temperatures. This hinders the enzymatic synthesis of compounds for which the thermodynamic equilibrium in aqueous solution is shifted in the unfavourable direction. Typical examples of such processes are syntheses of esters and peptides, polymerization of sugars, dehydration reactions, etc.

This variance could be successfully settled by using biphasic reaction media of the type "water - water-immiscible organic solvent" proposed to shift chemical

equilibria.^{15,16} The thermodynamics of the biphasic method has been analyzed in detail by our Moscow group. $17,18$ There are a few reviews on enzymatic syntheses carried out using the biphasic technique.^{1, 1972} Some peptides have been synthe sized under mild conditions in a high yield.²⁹⁻²⁰ Among the proteases used for peptide synthesis 80 far, oarboxypeptidase Y from yeast haa been a subject of special interest. ²⁸⁻³⁰ The biphasic method has undoubtedly started a novel sta ge^{31} in the development of synthesis of peptides.

Recently, the possibility of 100% yield in the biphasic enzymatic reaction has been questioned. $32,33$ We believe that this aim is well attainable if the conditions of synthesis are optimized. So far this problem had been settled only for the enzymatic synthesis of amino acid esters where the nature of organic sol vent¹⁷, pH, 34 reagent (alcohol) concentration, 35 and some parameters of biocata lyst³⁶ were varied. The present work endeavours to optimize the peptide synthesis. As an example²⁷ we have chosen the reaction:

 $N-Ac-L-Trp$ + L-LeuNH₂ $\longrightarrow N-Ac-L-Trp-L-LeuNH_2$ + H₂0 (1) catalyzed by α -chymotrypsin in the biphasic system water \sim ethyl acetate. We varied the "organic phase/aqueous phase" volume ratio, the pH value of aqueous phase, and the concentrations of starting reactants. The experiments were carried out using both free and immobilized enzyme.

RESULTS AND DISCUSSIOW

Kinetics of the product formation and stability of α -chymotrypsin under the reaction conditions. For free M-ohymotrypsin at a conoentration in the aqueous phase of 20 mg/ml, the dipeptide synthesis reached equilibrium only in 6-7 days. Fig. 1 shows, as an example, the kinetic curves l-3 for product accumulation (1) at various values of pH. The broken lines show the concentrations corresponding to the limiting yield of the dipeptlde.

While determining the yield of the reaction product, one should be sure that the horizontal part of the kinetic curve does correspond to the equilibrium of reaction (1) and is not caused by other factors, e.g., enzyme inactivation. In order to clarify this, we added a new portion of the enzyme to the aqueous phase and found no change in the content of the reaction product. Thus the horizontal part on curves 1-3 does correspond to the true equilibrium of reaction (1).

The reaction time shown in Fig. 1 corresponds to that for the synthesis catalyzed by free enzyme in the simplest biphasic system (see Experimental) oonslating of two mildly stirred maorolayers (water and ethyl acetate). The reaction time can evidently be altered by varying the catalyst concentration, the area of interfaoe, and the stirring rate. To increase significantly the interface, an emulsion of an aqueous enzyme solution in ethyl aoetate should be used. However, in this case the free enzyme becomes rather quickly Inactivated because of adsorption on the interface.

Therefore, the enzyme should be immobilized on or inside a support. To this end &-ohymatxypsin adsorbed on terephtalate granules (Sorsllen) was used. After immobllzation the enzyme becomes more stable, i.e. it eesentially does not inactivate during the synthesis and oan be used repeatedly (Fig. 2). Furthermore, intensive stirring (emulsifying) reduced the reaction time from a few days (for the free enzyme) to a few hours. However, when the immobilized enzyme preparation is used the synthesis time (rate of enzymatic reaction) is significantly dependent on the aarrier porosity and the surface concentration of catalytic sites. The results found for **x-chymotrypsin adsorbed on Sorsilen are completely in** line with earlier experimental data obtained by Nonsan's group for the asme enzyme covalently immobilized on Spherosil, ³⁶ and with theoretical conceptions^{27, 38}

Fig. 1. Kinetics of the dipeptide accumulation in reaction (1) proceeding in the biphasic system water - ethyl acetate. Conditions: $V_{\text{or}g}/V_{\text{a}q} = 50$, [AcTrp] = [LeuNH₂] = $= 10^{-3}$ M, enzyme concentration 20 mg per ml of aqueous phase.

Big. 2. Comparieon of stability of free and immobilized ∝-cnymo
sciss) r
…… otrypsln. α -chymotrypsin. The results for free enzyme (lower ab-
sciss) reflect its inactivation under the synthesis conditions given in Fig. 1 (pH 7). Immobilized enzyme (adsorbed on Sorsilen) is muoh.more stable and may be used repeatedly (upper abaciea); for the synthesis conditions, see Experimental.

Effect of the "organic phase/aqueous phase" volume ratio on the product yield. It follows from the theory of biphasic method^{17,18} that the reaction yield is dependent on the organic phase/aqueous phase volume ratio (V_{org}/V_{aq}) . The experimental data are presented in Fig. 3. The increase in the product yield with increasing V_{org}/V_{ag} ratio is accounted for by differences in partition coefficients of starting reactants and reaction products between organic and aqueous phases. More precisely, the solubility of the dipeptide in water is much lower than that of the starting amine and acid. Thus, the dipeptide formed in the course of enzymatic reaction is removed from the reaction medium (i.e. from aqueous phase) by being extracted into the organic solvent. Therefore, the equilibrium of the reaction is shifted toward the side of product formation, the shift being the greater the better extraction, i.e., the greater the "organic phase/aqueous phase" volume ratio $(Fig. 3).$

Effect of the pH of aqueous phase on the product yield. The dipeptide yield as a function of pH of the aqueous phase is shown in Fig. 4. The curve has a broad ma-18 ximum in agreement with the data reported earlier.

Effect of the concentrations of starting reactants on the product yield. The product yield of reaction (1) as a function of the concentrations of the starting reactants (N-acetyl-L-tryptophane and L-leucine amide) is shown in Pig. 5; the dipeptide yield increases with increasing concentrations of starting reactants.

Fig. 3. The dipeptide yield as a function of the "organic phase/aqueous phase" volume ratio. Conditions: $[ACTrp] = [LeuNH₂] = 10⁻³ M, concen$ tration of free α -chymotrypsin is
20 mg per ml of aqueous phase, pH 7.

Fig. 4. The dipeptide yield as a function of the pH value in aqueous phase, Conditions: $[AGTrp] = [LeuNH₂]$ = 10^{-3} M, concentration of free α chymotrypsin is 20 mg per ml of aque-
ous phase, $V_{org}/V_{aq} = 50$.

Fig. 5. The dipeptide yield as a function of the concentration of starting reactants. Solid curve ia calculated from equation (4) using the experimental value K = 3 x **10 . Con**ditions: $V_{\alpha r\alpha}/V_{\alpha\alpha} = 25$, pH 7, concentration of free \propto -chymotrypsin is 20 mg per ml of aqueous phase.

Fig. 6. Linearization of experimental data of Fig. 5 in **coordinates of equa**tion (4).

Equilibrium constant. Analysis of the dependence presented in Fig. 5 allows one to determine the equilibrium constant for reaction (1) :

$$
K = \frac{[A \circ Trp - I \circ e \circ N]_{eq} [H_2 O]_{eq}}{[A \circ Trp]_{eq} [I \circ \circ N]_{eq}}.
$$
 (2)

Using designations $[ACTrp - LeuNH₂] = P$, $[ACTrp] = [LeuNH₂] = g$ we obtain:

$$
K = \frac{P_{eq} [H_2 O]_{eq}}{a^2_{eq}} = \frac{P_{eq} [H_2 O]_{o}}{(a_o - P_{eq})^2}
$$
 (3)

where the index "o" denotes initial concentrations. T The assumption $[H_20]_{\alpha\alpha}$ equed to the H_2

 $[H_2O]$ is based on the fact that $[H_2O]$ \rightarrow P_{eq}, implying that a change in water concentration during the reaction can be neglected. Equation (3) may be rewritten **as**

$$
lg \frac{x [H_2 0]_0}{(1 - x)^2} = lg K + lg a_0
$$
 (4)

where $x = P_{eq}/a_q$ is the reaction yield. According to equation (4), the intercept of the plot lg $x[h_20]_{0}/(1 - x)^2$ ve lg a gives lg K (Fig. 6). The equilibrium constant thus determined is 3×10^{4} ; the K value in water is only about 10, 800 Ref. 37. The plot of the product yield **as a** function of the concentrations of starting reactants calculated from equation (4) using the determined value K = $= 3 \times 10^4$, is shown in Fig. 5 as a solid line.

Preparative enzymatlo eyntheeie. The experimental results obtained (Pige. *3-5)* **enable UB to formulate** the oondltione optimal for reaohing the maximum produot yield of reaotlon (1) in the biphaeic system water - ethyl aoetater the "organlo phase/aqueous phase" volume ratio *(Vorg/ Vaq) is more* than 50, the pH value of aqueous phaee Is from *6 to 9* and the oonoentrations of starting reactants are higher than 3 x 10^{-3} M (referred to the total volume of the system).

Under these conditions the preparative yield of N-acetyl-L-tryptophanyl-Lleucine amide in the biphasic system was practically 100%. In fact, 274 mg dipeptlde were obtained (from the organic phase only), whioh coincidee, within the experimental error, with theoretical yield. The purity of **the** product *waz* established by means of thin-layer chromatography. The amount of the dipeptide in the spot was determined spectrophotometrically (see Experimental). Furthermore, the product waz ehown to be chromatographically homogeneous; epota on a ohromatographio plate corresponding to starting reaotante were not detected at the end of the reaction.

Conolusion. Beyond any doubt, more experiments must be carried out to obtain detailed physicochemical description of the particular reaction system employed in the present study. For example, it would be neceseary to determine partition coeffloients of both eubetrates and the product between the two phaeee, to take into account the effect of pH and aubetratee oonoentratione on the ionization degree of both substrates and the product, the possibility of pH variation in the course of the reaction, eto. However, the main goal of the present **study wae just to** outline the general way or prooedure for searching optimal oonditions for enzyme-catalyzed syntheses In biphaalc syetems, and this goal was achieved quite Buccesefully.

WPERIMEKTAL

Materials. α -Chymotrypsin from bovine pancreas was product of Biokhimreaktiv (Olaine, Latvia). The content of the active *enzyme* in the preparation, determined as described by Bender's group⁴⁰, was 66%. N-Acetyl-L-tryptophane, L-leucine amide hydrochloride and B-aoetyl-L-tyrptophanyl-L-leucine amide was obtained from Reanal (Hungary). Ethyl acetate was a product of Reakhim (USSR).

Enzyme immobilization. To 0.5 ml 0.5 M phosphate buffer (pH 7), 0.5 g Sorsilen were added. The mixture waz deaerated under low pressure (10 mm Hg) and 10 mg d-ohymotrypsin added. The mixture was agitated for 30 min, the time sufficient for a complete adsorption of the enzyme. Characteristics of the terephtalate support (Sorsilen), produced at the Polymer Division of the Institute of Chemical Technology (Prague, Czechoslovakia) were reported earlier.⁴¹

Reaction catalyzed by the free enzyme. α -Chymotrypsin (20-40 mg/ml) was added to the solution of B-acetyl-L-tryptophane and L-leuclne emide hydroohlorlde, taken in equimolar concentrations (6 x 10⁻⁴ to 2 M), in 0.1 M acetate/phosphate/borate buffer, pH 7. The pH value of the solution changed, since commercial leucine amide was in a hydrochloride form and because of buffer properties of a-chymotrypsin. Therefore, pH of the solution was adjusted to the needed value every time after dlsaolving the reactants.

The buffer eolution **of** *reactants* with adjusted pH was placed in a flask and water-saturated ethyl acetate wae added to obtain the needed *"organic* phese/aqueoue phase" volume ratio. The total volume wae 10 to 100 ml. The reaotion mixture waa carefully agitated using a laboratory shaker 80 that not to allow emulsion to form.

It **ie to be** noted that, if it ia not indioated othezwise, everywhere in the text all ooncentratlone are referred to the total volume of the reaotion **system, i.e.** including both aqueoue and organic phaees.

Reaction catalyzed by immobilized α -chymotrypsin. Water-saturated ethyl acetate (8 ml) containing 0.008 M of both etarting reactants was **added to** the **buffer 8ue**pension of polymeric granules with adsorbed enzyme (see above). The reaction mixture was stirred at more than 160 r.p.m.

Determination of the reaction yield using thin-layer chromatography. Aliquotes of organic phase were taken from the biphasic reaction mixture in certain time intervale. To determine the product yield, the aliquote of organic phase (0.05 to 4.5 ml) was plaeed on a 5 x 15 om Silufol chrcmatographlc plate (Czechoslovakia) which was placed into elution camera containing a mixture of propyl alcohol and aqueous ammonia (7 : 3 v/v). The chromatography was performed using the ascending elution technique and employing commercial N-aoetyl-L-tryptophanyl-L-leucine amide as a marker. After drying the chromatographic plate a 2×5 om strip was cut out off at the level corresponding to the R_{ρ} value of the reaction product (0.87). The strip was cut to small pieces which were placed into 4 ml dietilled water to wash off the dipeptide. The aqueous solution was separated In a day by centrifugation and the concentration of the product was measured spectrophotometrically at 280 nm (molar absorbance being $6.5 \times 10^3 \text{ M}^{-1}$ cm⁻¹, see Ref. 42).

Determination of the relative catalytic activity of α -chymotrypsin in the course of reaction. In certain time intervals aliquotes (0.01 to 0.1 ml) were withdrawn from the aqueous phaae of the reaation mixture and plaaed into a epectrophotometer cell containing 2 ml 0.1 M acetate/phosphate/borate buffer at pH 7 and 0.02 ml 1.3×10^{-2} M N-3-carboxypropionyl-L-phenylalanine-p-nitroanilide in the acetonltrlle-dioxane (1 : **1 v/v)** mixture. The a-chymotryptic hydrolyeis of this specific substrate⁴³ was followed at 380 nm by the rate of appearance of p-nitroaniline.

Preparative synthesis of N-aaetyl-L-tryptophanyl-L-leualne amide. The preparative synthesis of the dipeptide was performed in the biphasic system containing 1 ml of 0.1 M acetate/phosphate/borate buffer (pH 7) and 100 ml of water-saturated ethyl acetate. The aqueous phase contained 0.01 M of both N-acetyl-Ltryptophane and L-leucine amide hydrochloride and 20 mg/ml α -chymotrypsin. The synthesis was carried out with careful agitation of the reaction mixture in a laboratory shaker. After the reaction completed, the organic phase was separated and ethyl acetate removed in vacuo. The preparation should be dried under reduced pressure over P_2O_F at room temperature for three days to obtain satisfactory results of elemental analysis.

Spectrophotometric measurements were made on a Beckman-25 lnetrument.

Acknowledgement. The authors wish to express their gratitude to Professor I.V. Berezin for his comments and to Dr. J.Turkova for her invaluable aid in developing the method of enzyme immobilization on Sorsilen.

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